In the Claims:

Please amend the claims as follows.

- (Currently Amended) A process for making multiple grades of base oil products, wherein said process comprises the following steps:
- (a) hydrocracking a mineral crude derived feed, thereby obtaining an effluent;
- (b) distilling of the effluent as obtained in step (a) into at least one middle distillates product and a full range residue boiling substantially above 340 °C;
- (c) catalytically dewaxing the full range residue by contacting the full range residue with a dewaxing catalyst comprising a dealuminated extrudate of a zeolite of the MTW type and a low acidity refractory binder material wherein the weight ratio of said zeolite to said low acidity refractory binder material is in the range of from 5:95 to 95:5 and a Group VIII metal of either platinum or palladium that is present in said dewaxing catalyst in the range of from 0.1 to 5.0% by weight, thereby obtaining a dewaxed oil;
- (d) isolating by means of distillation two or more base oil grades from the dewaxed toil obtained in step (c); and
- (e) isolating a dewaxed gas oil from the dewaxed oil obtained in step (c); wherein the dewaxed oil as obtained in step (c) comprises between 10 and 40 wt% of a dewaxed heavy gas oil boiling for more than 70 wt% between 370 and 400 °C.
- (Previously Presented) The process according to claim 1, wherein more than 20 wt% of the mineral crude derived feed to step (a) boils above 470 °C.
- 3. (Previously Presented) The process according to claim 2, wherein a fraction of the dewaxed gas oil is recycled to step (b) to be mixed with the effluent before distilling thereof.
- 4. (Previously Presented) The process according to claim 3, wherein from 0 to 15 wt% of the full range residue as obtained in step (b) is recycled to step (a) to be mixed with the mineral crude derived feed before hydrocracking thereof.

- 5. (Previously Presented) The process according to claim 4, further comprising adding a Fischer-Tropsch derived partly isomerised paraffin fraction to the full range residue prior to catalytically dewaxing.
- 6. (Currently Amended) The process according to any one of claim 5, wherein the dewaxed oil of step (c) is subjected to an additional hydrofinishing step.
- 7. (Previously Presented) The process according to claim 6, wherein the hydrogen partial pressure in step (c) is greater than 100 bars.
- 8. (Currently Amended) The process according to claims 7, wherein the base oil grades obtained in step (d) each comprises more than 95 wt% saturates and have a viscosity index of between 95 and 120.
- 9. (Previously Presented) A dewaxed gas oil made by the process of claim 1.
- 10. (Previously Presented) A dewaxed gas oil according to claim 9, wherein the gas oil has an aromatic content of below 0.1 mmol/100 grams, a sulphur content of below 10 ppm and a pour point of below -30 °C.
- 11. (Canceled)